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Research Article

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Influence of interfacial electrokinetic on MHD radiative nanofluid flow in a permeable microchannel with Brownian motion and thermophoresis effects

https://doi.org/10.1515/phys-2020-0161 received May 12, 2020; accepted August 22, 2020

Abstract: In this study, the behavior of a microchannel flow is examined. The fluid is considered to be a nanofluid, which moves between two parallel flat plates in the presence of an electrical double layer. The Buongiorno nanofluid is considered with body force. In this study, the unphysical supposition presented in the preceding work to the discontinuity of the flow fled where the electrostatic potential in the central of the canal must be equal to zero is removed. The incorrect supposition that the pressure constant is preserved, which is considered a known form, is corrected. The current fresh model equation is modified by using dimensionless parameters to convert partial differential equations into ordinary differential equations. The transformed nonlinear equations are solved by the homotopy analysis method. The physical parameters, magnetic parameters, Eckert number, Lewis number, Brownian

motion parameters, thermophoresis parameters, and Prandtl number are analyzed. The influence of both the viscous and Joule dissipation in the presence of magnetohydrodynamic effect is examined.

Keywords: nanofluid, electrical double layer, microchannel, similarity transformation, HAM

1 Introduction

Nanofluid contains nanometer-sized particles called nanoparticles. Nanofluids are formed by the colloidal interruptions of nanoparticles in a base fluid. Nanofluids have low thermal conductivity and therefore do not attain the required freezing or heating rates. To overcome this challenge, nanoparticles are inserted in base fluids. This increases the heat transfer characteristics of nanofluids which find applications in a wide range of industrial settings such as nuclear power plants, paper production, vehicle cooling, and domestic fridges.

We know that the industrial and viscous fluids differ in their various rheological features. This type of fluid is called non-Newtonian fluid. This type of fluid has numerous applications in various fields, such as plastic manufacturing, wire coating, paper and fabric vanishing, polymer production, and food dispensation. Characterizing the behavior of such type of fluids is difficult by simply using Navier-Stokes equation. This means there is no unique relation that shows the exact behavior of the non-Newtonian fluids. Therefore, many authors propose different models of non-Newtonian fluids. In this study, we discuss the Williamson fluid model [1]. He found that this type of fluids has unique characteristics which ideal plastic and viscid fluids do not possess.

One of the primary problems of the globe is maintaining energy generation. Sunlight-based vitality gives the results the hourly sun oriented transition on the earth surface being more notable than most of the human utilization of vitality in a year. Focusing on the sunlightbased vitality has been one of the most important and interesting areas for the researchers in the past few years.

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Recently, a research study suggests that adding nanoparticles to the nanofluids increases heat transmission and solar collection. Solar energy is the best source of energy due to its negligible impact on the environment [2]. One of the essential elements in our daily life is solar energy through which we get electricity, heat, and water. Nanoparticles are an important topic of recent research. Nanofluids are heat transmission fluids which comprise a base fluid and nanoparticles. The purpose of using nanoparticles is to increase the heat transmission of the base fluid [3]. The thermal conductivity of the base liquid increases by the Brownian motion of the nanoparticles. Magnetohydrodynamic (MHD) nanofluids have vital implications in physics, chemistry, and engineering. The MHD flow of nanofluids with radiation heat transmission and movable surface heat flux in porous media is discussed by Zhang et al. [4].

This is why the subject of heat transmission in nanofluids is of much attraction to the authors. Choi and Eastman [5] have introduced the concept of nanofluid and showed that the thermal properties of the base liquids improve significantly once nanoparticles are introduced. Despite the groundbreaking struggle, the effects of theapplication of nanoparticles to fluid flow are being explored by many scientists. Sheikholeslami et al. [6] investigated the 3D nanofluid force in the presence of a magnetic field using lattice Boltzmann method. Nithyadevi et al. [7] discussed the effect of the angle of inclination on the mixed convection of the nanofluid. Dhananjay et al. [8] studied the isothermal boundary condition of the nanoparticles in the presence of Lorentz force. Selimefendigil and Hakan [9] used the finite element method to examine the heat transfer in conjugate natural convection-condition. Hayat et al. [10] showed the impact of radioactivity on nanofluid concentrations. They showed that heat dispersion increases with an increase in thermal radioactivity. Sheikholeslami [11] studied the motion of the nanofluid in a porous semi-annulus under the influence of a magnetic field. Sheikholeslami et al. [12] investigated a two-phase nanofluid in the presence of an unsteady magnetic field. They used the homotopy perturbation method for solving the model equation. Farooq et al. [13] studied the MHD Falkner-Skan flow of the nanofluid. Shehzad et al. [14] discussed about Jeffrey nanofluid with internal heat. Abbasi et al. [15] investigated Jeffrey nanofluid under heat and mass flux conditions.

Due to various applications and consideration of microchannel flow, Kandlikar and Grande [16], Bergles et al. [17], and Thome et al. [18] introduced some alternative ways of cooling microsized devices. High applications of microchannel heat sinks using large-scale cooling microreactors for the study of organic cells and the microfluid pumps have been discussed by Safaei et al. [19] and Arani et al. [20]. Particularly, Wang and Peng [21] found that the transmission and laminar heat transformation in microchannels is strange and quite complex with a conservatively sized condition. Zhao et al. [22] discussed the heat transfer investigation of the nanofluid flow in a microchannel. Recently, some researchers studied the heat transfer flow of nanofluids for different purposes [23-33]. Anum et al. [34–36] studied mass transfer and heat transfer of Williamson and Walters-B nanofluid flow with MHD and thermal radiation. Sunil et al. [37-39] investigated the fractional Lotka-Volterra model in the Caputo sense. They converted the considered modelled equation into an algebraic equation to solve it easily. They also discussed a model to describe the velocity of the particle during Brownian motion. Khalid et al. [40] introduced an analytical and numerical study of the Peyrard-Bishop DNA dynamic model. They compared the analytical and numerical results and presented in graphs. Lu et al. [41] studied the numerical and analytical simulation of the separation phase for the ternary alloys of iron. Hadi et al. [42] used the method of exponential rational function to solve four conformable fractional Boussinesq-like equations. Osman et al. [43-47], Ahmad et al. [48], and Omar et al. [49] used the unified technique and the modified reproducing kernel discretization technique to solve different model equations. They showed that the unified method offers a powerful mathematical tool to solve the nonlinear conformable fractional evaluation equations. Jian-Guo et al. [50] studied the Hirota equation and found an exact solution. Sumit et al. [51-53] investigated the heat and mass transfer of the two-dimensional flow. The fluid they considered in their work is Williamson nanofluid with MHD. Prakash et al. [54] discussed the thermal radiation of the nanofluid flow in the presence of peristalsis electroosmosis phenomenon. The tapered asymmetric microchannels were taken into account in his work. Sharma et al. [55] investigated the MHD mixed convection flow of the non-Newtonian fluid. Gupta and Dutta [56] examined a mathematical model for HIV/AIDS and solved using the homotopy analysis method (HAM). For comparing the accuracy, they used the numerical method.

In the light of these studies, the main aim of this research is to examine the nanofluid flow of the Williamson fluid. The fluid here in this study moves between the two parallel flat plates in the presence of an electrical double layer (EDL). The Buongiorno nanofluid is considered with body force. In this study, the unphysical supposition presented in the preceding work to the discontinuity of the flow fled where the electrostatic potential in the central of the canal must be equal to zero is removed. The physical parameters have been analyzed and discussed. The influence of both the viscous and Joule dissipation in the presence of MHD effect is examined. We choose the HAM method to solve this problem. The purpose of choosing this method is that it is a fast convergent and time-saving method and offers the choice of choosing our own auxiliary linear operator. HAM is an analytical method, which is semianalytical. We solved nonlinear ordinary differential equations by using HAM. The stated technique pays the conception of the homotopy taken from the topology, and it generates a convergent series result for nonlinear systems. This is supported by operating a homotopy Maclaurin series to compact with the nonlinearities in the system. Jagdev et al. [57,58] used a numerical scheme q-local fractional homotopy analysis transform method to solve the local fractional linear transport equation. Gupta et al. [59,60] and Das et al. [61] used HAM and a new powerful algorithm based on HAM to solve the nonlinear diffusion equation.

1.1 Analytical solution to the electrostatic potential

Viscous and Joule dissipation MHD.

The ratio between $\overset{*}{\Omega}$ and ρ_{e} is given below:

$$D_{yy} \stackrel{*}{\Omega} = -\frac{\rho_e}{\omega_o \omega},\tag{1}$$

where ω represents the dielectric constant and ω_o represents the permittivity of the vacuum of the fluid.

Manipulating the hypothesis of the equilibrium Boltzmann dispersal around the unchanging dielectric constant and omitting the variation, the number of the ion dissemination in the symmetric electrolyte result is given by

$$n_i = n_{0i} \exp \left(-\frac{\widehat{z}_i e \Omega}{k_b \widehat{T}}\right), \qquad (2)$$

where η_{0i} signify the bulk ion concentrations and \hat{z}_i signify the valence of the *i* type ions. The charge of a proton is denoted by *e*, Ω represents the electrical potential, k_b is the Boltzmann constant, and \hat{T} represents the total temperature. In a unit volume of the fluid, the average charge density is

$$\rho_e = (n_+ - n_-)\widehat{z}_i e = -2n_0\widehat{z}_i e \sinh\left(\frac{\widehat{z}_i e\Omega}{k_b\widehat{T}}\right).$$
(3)

By simulating equation (3) into equation (1) (Poisson's equation), we get the famous Poisson–Boltzmann equation:

$$\frac{\mathrm{d}^2 \hat{\Omega}}{\mathrm{d} y^2} = \frac{2n_0 \widehat{z}_i e}{\omega_0 \omega} \sinh\left(\frac{\widehat{z}_i e \hat{\Omega}}{k_b \widehat{T}}\right). \tag{4}$$

By applying the similarity transformation, we get the nondimensionalized form of equation (4):

$$X = \frac{x}{H}, \quad Y = \frac{y}{H}, \quad \Omega(Y) = \frac{\widehat{z}_i e \Omega}{k_b \widehat{T}}, \quad \rho^* = \frac{\rho_e}{n_0 \widehat{z}_i e}, \quad (5)$$

$$\frac{\mathrm{d}^2\Omega}{\mathrm{d}Y^2} = \kappa^2 \,\sinh(\Omega(Y)),\tag{6}$$

$$\frac{\mathrm{d}^2\Omega}{\mathrm{d}Y^2} = -\frac{\kappa^2}{2}\rho^*(Y),\tag{7}$$

where $\kappa = Hk$ in which $\kappa^2 = \frac{2n_0 \hat{z}_i^2 e^2}{(\omega_0 \omega k_b \hat{T})}$ represents the Debye– Hückel parameter, and $1/\kappa$ represents the thickness of the EDL. A suitable boundary condition for equations (6) and (7) is given below:

$$\Omega(\pm 1) = \bar{\xi} = \frac{\widehat{z} e \xi}{k_b \widehat{T}},\tag{8}$$

where ξ is the zeta potential which is used for the measurement of the electrical potential at the shear plane, i.e., the horizon in between diffuse film and compacted film [10].

If the electric potential is lesser than the thermal energy of the ions, i.e., $(|\widehat{z} e \Omega|) \ll |k_b \widehat{T}|$, using Debye–Hückel linear approximation, equation (6) becomes

$$\frac{\mathrm{d}^2\Omega}{\mathrm{d}Y^2} = \kappa^2 \Omega(Y). \tag{9}$$

Analytically, it is given by

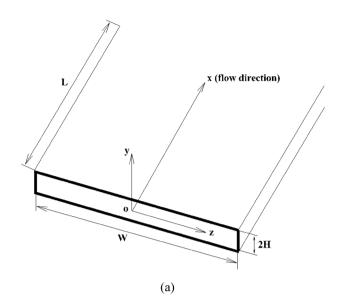
$$\Omega(Y) = \frac{\bar{\xi}}{1 + e^{2k}} [e^{\kappa(1+Y)} + e^{\kappa(1-Y)}].$$
(10)

1.2 Mathematical formulation for other fields

We use horizontal rectangular microchannel with EDL and pass the nanofluid flow of heat transmission over the stated microchannel. Figure 1 shows the physical effect. *X*-axis is parallel to the channel of the walls, and *Y*-axis is perpendicular to the walls. We keep the origin fix here at the center line of the microchannel. *H* denotes half distance between the upper and the lower wall. Length and width of the microchannel are denoted by *L* and *W*, respectively. For simplification, consider $W \gg H$. Then, we can frame the current research problem as a nonlinear microchannel flow of two-dimension with the effect of EDL:

$$\nabla \cdot V = 0, \tag{11}$$

$$\rho(V \cdot \nabla) V = -\nabla p + \mu \nabla^2 V + F, \qquad (12)$$



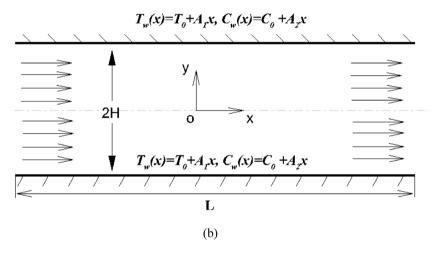


Figure 1: Geometry of the current problem: (a) geometry in 3D and (b) geometry in 2D.

$$(V \cdot \nabla) T = \alpha \nabla^2 T + \tau \left[D_B \nabla T \cdot \nabla C + \left(\frac{D_T}{T_0} \right) \nabla T \cdot \nabla T \right]$$
(13)
+ $\frac{\mu}{\rho c} \Phi$,

$$(V. \nabla)C = D_B \nabla^2 C + \left(\frac{D_T}{T_0}\right) \nabla^2 T, \qquad (14)$$

where *F* is the electrical body force and Φ is the viscous dissipation term, which is defined as

$$\Phi = 2[(u_x)^2 + (v_y)^2 + (w_z)^2] + (v_x + u_y)^2 + (w_y + v_z)^2 + (u_z + w_x)^2 - \frac{2}{3}(u_x + v_y + w_z)^2.$$
 (15)

If the flow is parallel in the channels, then only one component of the velocity field will not be zero. This means that the collective fluid particles move in a similar path. Only the velocity part *u* is nonzero; therefore, *v* is zero in all places. From the continuity equation, $u_x = 0$; thus, *u* is independent of *x*. In the same way, the hydraulic pressure, which is represented by *p*, is only dependent on the motion of the fluid, which shows that it is only a function of *x*, and thus the pressure gradient p_x is a constant. It is presumed that the volumetric fraction of the temperature and the nanoparticle on both walls rise or fall linearly with *x*, namely, $T_w(x) = T_0 + A_1x$ and $C_w(x) = C_0 + A_2x$, where T_0 represents the reference temperature and C_0 represents the volumetric fraction of the reference nanoparticle at the channel entrance. As the temperature *T* and volumetric fraction of the nanoparticle *C* vary linearly with *x* [21,22], we obtain $T_{xx} = C_{xx} = 0$. With the above supposition, we see that the continuity equation is satisfied, and rest of the governing equations are simplified to the following equations:

$$\mu u_{yy} - \frac{\sigma B_0^2}{\rho} u - \frac{v}{k} u - p_x + E_x \rho_e = 0, \qquad (16)$$

$$u_{x}T = \alpha T_{yy} + \tau D_{B} (T_{x}C_{x} + T_{y}C_{y}) + \frac{\tau D_{T}}{T_{0}} [(T_{x})^{2} + (T_{y})^{2}] + \frac{\mu}{\rho c} (u_{y})^{2} - \frac{\sigma B_{0}^{2}}{\rho C_{p}} u^{2},$$
⁽¹⁷⁾
$$uC_{x} = D_{B}C_{yy} + \frac{D_{T}}{T_{0}}T_{yy},$$
⁽¹⁸⁾

using the boundary conditions

$$u(\pm H) = 0, \quad T_w(\pm H) = T_0 + A_1 x, C_w(\pm H) = C_0 + A_2 x.$$
(19)

In the channel flow study, we assumed the mass flow rate as a given number. Therefore, we get the following:

$$V_m = \frac{1}{2H} \int_{-H}^{+H} u(y) dy = \frac{1}{H} \int_{0}^{+H} u(y) dy, \qquad (20)$$

where U_m denotes the average fluid velocity passing through the channel section. Using the dimensionless parameters,

$$V(Y) = \frac{u}{V_m}, \quad \Theta(Y) = \frac{T - T_0}{A_1 H}, \quad \Phi(Y) = \frac{C - C_0}{A_2 H}.$$
 (21)

Nondimensionalizing equation (16) by similarity transformations (5) and (21), we get

$$\frac{\mathrm{d}^2 V}{\mathrm{d}Y^2} - K_1 - 2K_2\overline{E}_s\Omega(Y) - MV - KV = 0. \tag{22}$$

Using boundary conditions

$$V(\pm 1) = 0, \quad V \int_{0}^{1} V(Y) dY = 1,$$
 (23)

where $K_1 = \frac{H^2}{\mu V_m} P_x$, $K_2 = \frac{n_0 \widehat{z} e \xi H^2}{\mu V_m L}$, where $P_x = -\partial p / \partial x$ represents the pressure constant, $\overline{E}_s = E_s / \xi$ is the stream potential, $E_x = E_s / L$.

Substituting the nondimensional variables (21) into equations (17) and (18), we get the compact energy and concentration of nanoparticle equations as

$$\frac{d^{2}\Theta}{dY^{2}} + Nb\left(1 + \frac{d\Theta}{dY}\frac{d\Phi}{dY}\right) + Nt\left(1 + \left(\frac{d\Theta}{dY}\right)^{2}\right)$$

$$+ \operatorname{PrEc}\left(\frac{dV}{dY}\right)^{2} - \operatorname{Re}\operatorname{Pr}V - J(V)^{2} = 0,$$

$$\frac{d^{2}\Phi}{dY^{2}} + \frac{\operatorname{Nt}}{\operatorname{Nb}}\frac{d^{2}\Theta}{dY^{2}} - \operatorname{Re}\operatorname{PeLeV} = 0,$$
(25)

subject to the boundary conditions

$$\Theta(\pm 1) = 0, \quad \Phi(\pm 1) = 0,$$
 (26)

where Nb = $\frac{\tau D_B A_2 H}{\alpha}$ is the Brownian motion parameter, Nt = $\frac{\tau D_T A_1 H}{\alpha T_0}$ is the thermophoresis parameter, Pr = $\frac{V_m}{\alpha}$ is the Prandtl number, Re = $\frac{V_m H}{\nu}$ is the Reynolds number, Ec = $\frac{V_m^2}{cA_1 H}$ is the Eckert number, Le = $\frac{\alpha}{D_B}$ is the Lewis number, $M = \frac{H^2 \sigma B_0^2}{\mu \rho}$ is the magnetic parameter, $k = \frac{H^2 \nu}{\mu \kappa}$ is the permeability parameter, and $J = \frac{H \alpha B_0^2}{\alpha A_1 \rho c_p}$ is a Joule dissipation term.

The main physical quantities of practical interests are the local skin friction, the local Nusselt number, and the local Sherwood number. We know that the flow inside the channel is a symmetric flow; therefore, we can consider them on the lower plate. Therefore, in the current situation, it is defined as

$$C_{f2} = \frac{\tau_{w2}}{\rho_f V_m^2}, \text{ Nu}_2 = \frac{xq_{wT2}}{k_f(T_w - T_0)}, \text{ Sh}_2 = \frac{xq_{wC2}}{D_B(C_w - C_0)},$$
(27)

where

$$\tau_{w2} = \mu u_{yy=-H}, \quad q_{wT2} = -k_f T_{yy=-H}, \quad (28)$$
$$q_{wC2} = -D_B C_{yy=-H}.$$

Substituting equation (21) into equation (27), we get the following:

$$C_{f2} = \frac{1}{\text{Re}}V'(-1), \text{ Nu}_2 = -\Theta'(-1), \text{ Sh}_2 = -\Phi'(-1).$$
 (29)

1.3 HAM solution

We solve equations (9) and (22)–(25) using the given boundary conditions (8), (23), and (26). We use HAM in the succeeding way.

The linear operators are taken as

$$L_{\Omega}(\Omega) = \Omega'', \quad L_{V}(V) = V'', \quad L_{\theta}(\theta) = \theta''$$

and $L_{\varphi}(\varphi) = \varphi'',$ (30)

containing the following characteristics:

$$L_{\Omega}(c_1 + c_2\eta) = 0, \quad L_V(c_3 + c_4\eta) = 0,$$

$$L_{\theta}(c_4 + c_6\eta) = 0, \quad L_{\varphi}(c_7 + c_8\eta) = 0,$$
(31)

where c_i (*i* = 1–8) are constants.

The initial assumptions are selected as follows:

$$\Omega_0(\eta) = \eta, \quad V_0(\eta) = 0, \quad \theta_0(\eta) = 0, \quad \varphi_0(\eta) = 0.$$
 (32)

The resulting nonlinear operators N_{Ω} , N_V , N_{θ} , N_{φ} are given as follows:

$$N_{\Omega}[\Omega(\eta;p)] = \frac{\partial^2 \Omega(\eta;p)}{\partial \eta^2} - k^2 \Omega(\eta;p), \qquad (33)$$

$$N_{V}[V(\eta;p), \Omega(\eta;p)] = H^{2} \frac{\partial^{2} V(\eta;p)}{\partial \eta^{2}}$$

- $K_{1} - 2K_{2}E_{s}\Omega(\eta;p) - MV(\eta;p),$ (34)

$$N_{\theta}[V(\eta;p), \theta(\eta;p), \varphi(\eta;p)] = \left(1 + \frac{4}{2}Rd\right)\frac{\partial^{2}\theta(\eta;p)}{\partial\eta^{2}}$$
$$- N_{b}\left(1 + \frac{\partial\theta(\eta;p)}{\partial\eta}\frac{\partial\varphi(\eta;p)}{\partial\eta}\right)N_{t}\left(1 + \left(\frac{\partial\theta(\eta;p)}{\partial\eta}\right)^{2}\right) (35)$$
$$+ \operatorname{PrEc}\left(\frac{\partial V(\eta;p)}{\partial\eta}\right)^{2} - \operatorname{PrReV}(\eta;p)$$
$$- \operatorname{PrEcM}(V(\eta;p))^{2},$$
$$\partial^{2}\theta(\eta;p)$$

$$N_{\varphi}[V(\eta;p), \theta(\eta;p), \varphi(\eta;p)] = \frac{\partial^{2} \varphi(\eta;p)}{\partial \eta^{2}} + \frac{N_{t}}{N_{b}} \frac{\partial^{2} \theta(\eta;p)}{\partial \eta^{2}} - \operatorname{Re} PeLeV(\eta;p).$$
(36)

The detailed HAM method is discussed in ref. [1]. Here, zeroth-order problems are

$$(1-p)L_{\Omega}[\Omega(\eta;p) - \Omega_{0}(\eta)] = p\hbar_{\Omega}N_{\Omega}[\Omega(\eta;p)], \quad (37)$$

$$(1-p)L_V[V(\eta;p) - V_0(\eta)] = p\hbar_V N_V[V(\eta;p), \psi(\eta;p)], (38)$$

$$(1-p)L_{\theta}[\theta(\eta;p) - \theta_{0}(\eta)] = p\hbar_{\theta}N_{\theta}[V(\eta;p), \theta(\eta;p), \phi(\eta;p), \phi(\eta;p)],$$
(39)
$$\varphi(\eta;p)],$$

$$(1-p)L_{\varphi}[\varphi(\eta;p) - \varphi_{0}(\eta)] = p\hbar_{\varphi}N_{\varphi}[V(\eta;p), \theta(\eta;p), \qquad (40)$$
$$\varphi(\eta;p)].$$

The equivalent boundary conditions are

$$\Omega(\eta;p)|_{\eta=-1} = \xi, \quad \Omega(\eta;p)|_{\eta=1} = \xi, V(\eta;p)|_{\eta=-1} = 0, \quad V(\eta;p)|_{\eta=1} = 0, \theta(\eta;p)|_{\eta=-1} = 0, \quad \theta(\eta;p)|_{\eta=1} = 0, \varphi(\eta;p)|_{\eta=-1} = 0, \quad \varphi(\eta;p)|_{\eta=1} = 0,$$
(41)

where $p \in [0, 1]$ is the imbedding parameter, $h_{\Omega}, h_V, h_{\theta}, h_{\varphi}$ are used to control the convergence of the solution. When p = 0 and p = 1, we have

$$\Omega(\eta;1) = \Omega(\eta), \quad V(\eta;1) = V(\eta), \\ \theta(\eta;1) = \theta(\eta) \text{ and } \varphi(\eta;1) = \varphi(\eta),$$
(42)

expanding $\Omega(\eta;p)$, $V(\eta;p)$, $\theta(\eta;p)$, $\varphi(\eta;p)$ in Taylor's series about p = 0:

$$\Omega(\eta;p) = \Omega_0(\eta) + \sum_{m=1}^{\infty} \Omega_m(\eta) p^m,$$

$$V(\eta;p) = V_0(\eta) + \sum_{m=1}^{\infty} V_m(\eta) p^m,$$

$$\theta(\eta;p) = \theta_0(\eta) + \sum_{m=1}^{\infty} \theta_m(\eta) p^m,$$

$$\varphi(\eta;p) = \varphi_0(\eta) + \sum_{m=1}^{\infty} \varphi_m(\eta) p^m,$$
(43)

where

$$\Omega_{m}(\eta) = \frac{1}{m!} \frac{\partial \Omega(\eta; p)}{\partial \eta} \Big|_{p=0},$$

$$V_{m}(\eta) = \frac{1}{m!} \frac{\partial V(\eta; p)}{\partial \eta} \Big|_{p=0},$$

$$\theta_{m}(\eta) = \frac{1}{m!} \frac{\partial \theta(\eta; p)}{\partial \eta} \Big|_{p=0}, \quad \varphi_{m}(\eta) = \frac{1}{m!} \frac{\partial \varphi(\eta; p)}{\partial \eta} \Big|_{p=0}.$$
(44)

We choose the secondary constraints h_{Ω} , h_V , h_{θ} , h_{φ} in the way that the series (43) converges at p = 1. Switching p = 1 in (43), we get the following:

$$\Omega(\eta) = \Omega_0(\eta) + \sum_{m=1}^{\infty} \Omega_m(\eta),$$

$$V(\eta) = V_0(\eta) + \sum_{m=1}^{\infty} V_m(\eta),$$

$$\theta(\eta) = \theta_0(\eta) + \sum_{m=1}^{\infty} \theta_m(\eta),$$

$$\varphi(\eta) = \varphi_0(\eta) + \sum_{m=1}^{\infty} \varphi_m(\eta).$$
(45)

The *m*th order problem fulfills

$$L_{\Omega}[\Omega_{m}(\eta) - \chi_{m}\Omega_{m-1}(\eta)] = \hbar_{\Omega}R_{m}^{\Omega}(\eta),$$

$$L_{V}[V_{m}(\eta) - \chi_{m}V_{m-1}(\eta)] = \hbar_{V}R_{m}^{V}(\eta),$$

$$L_{\theta}[\theta_{m}(\eta) - \chi_{m}\theta_{m-1}(\eta)] = \hbar_{\theta}R_{m}^{\theta}(\eta),$$

$$L_{\varphi}[\varphi_{m}(\eta) - \chi_{m}\varphi_{m-1}(\eta)] = \hbar_{\varphi}R_{m}^{\varphi}(\eta).$$
(46)

The analogous boundary conditions are as follows (Figures 2 and 3):

$$\Omega_m(-1) = \Omega_m(1) = V_m(-1) = V_m(1) = 0,$$

$$\theta_m(-1) = \theta_m(1) = \varphi_m(-1) = \varphi_m(1) = 0.$$
(47)

Here,

$$R_m^{\Omega}(\eta) = \Omega_{m-1}'' - k^2 \Omega_{m-1}, \qquad (48)$$

$$R_m^V(\eta) = H^2 V_{m-1}'' - K_1 - 2K_1 E_s \Omega_{m-1} - M V_{m-1}, \qquad (49)$$

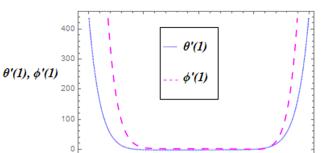


Figure 2: Combined *h*-curve graph of the temperature and concentration profiles.

h_{0,¢}

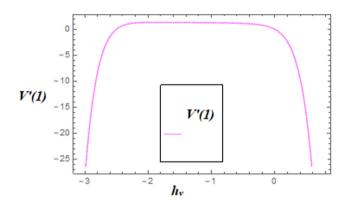


Figure 3: h-curve graph of the velocity profile.

$$R_{m}^{\theta}(\eta) = \left(1 + \frac{4}{2}Rd\right)\theta_{m-1}'' + N_{b}\left(1 + \sum_{k=0}^{m-1}\theta_{m-1-k}'\varphi_{k}'\right)$$
$$\times N_{b}\left(1 + \sum_{k=0}^{m-1}\theta_{m-1-k}'\varphi_{k}'\right)\operatorname{PrEc}\left(\sum_{k=0}^{m-1}V_{m-1-k}'V_{k}'\right)(50)$$
$$-\operatorname{PrRe}V_{m-1} - \operatorname{PrEc}M\sum_{k=0}^{m-1}V_{m-1-k}V_{k},$$
$$R_{m}^{\theta}(\eta) = \varphi_{m-1}' + \frac{N_{t}}{N_{b}}\theta_{m-1}'' - \operatorname{RePeLe}V_{m-1}, \qquad (51)$$

where

$$\chi_m = \begin{cases} 0, & \text{if } p \le 1 \\ 1, & \text{if } p > 1 \end{cases}$$

Figures 4 and 5 show the influence of $\kappa 1$ and $\kappa 2$ on velocity distribution V(Y). An increasing behavior is noticed for both $\kappa 1$ and $\kappa 2$. The higher value of $\kappa 1$ and $\kappa 2$ augmented the velocity of nanofluid flow.

The Hartmann number is based on the Lorentz force theory. As stated by the Lorentz force theory, the larger Hartmann number means more collision among the atoms of the fluid, which produces more resistive force to fluid

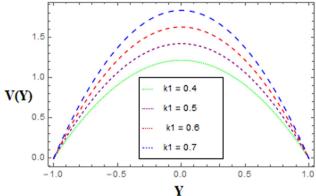


Figure 4: Variations in velocity distribution V(Y) for different values of $\kappa 1$.

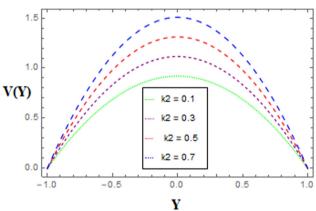


Figure 5: Variations in velocity distribution V(Y) for different values of $\kappa 2$.

flow. More opposing force reduces the fluid flow, and the velocity field falls down (Figure 6).

Figure 7 shows the Eckert number "Ec" on temperature distributions. We see that with increasing Ec, the thickness of the thermal boundary layer and temperature increase. When Ec increases, the energy of the heat is stored in the fluid, which is due to the friction forces that improve the temperature distribution.

Figure 8 shows that with increasing Lewis number, the concentration of the nanoparticle decreases, which correlates with the boundary layer thickness. It is because the Lewis number contains the coefficient of the Brownian dispersion. The coefficient of the Brownian dispersion is stronger for smaller values of the Lewis number and weaker for greater values of the Lewis number. Such type of weaker Brownian dispersion coefficient leads to a lower nanoparticle concentration distribution function.

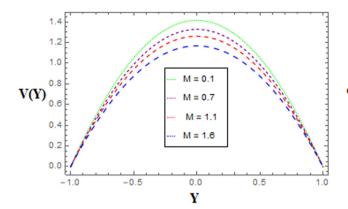


Figure 6: Variations in velocity distribution V(Y) for different values of *M*.

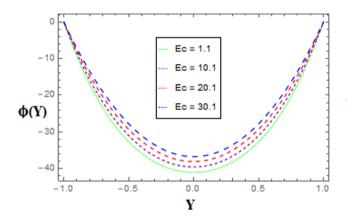


Figure 7: Variations in concentration distribution $\phi(Y)$ for different values of Ec.

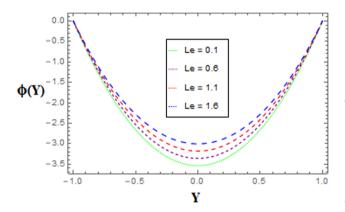


Figure 8: Variations in concentration distribution $\phi(Y)$ for different values of Le.

Figure 9 shows that higher Brownian motion causes arbitrary motion of the particles. Due to this arbitrary motion, extra heat is created. Thus, the reduction in concentration filed is depicted.

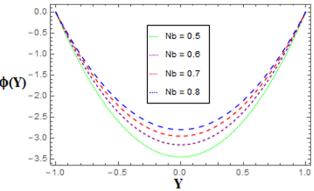


Figure 9: Differences in the concentration distribution $\phi(Y)$ for different values of Nb.

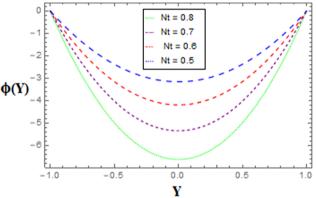


Figure 10: Variations in concentration distribution $\phi(Y)$ for different values of Nt.

Figure 10 shows that increasing Nt increases the concentration field, whereas in thermophoresis phenomena, small particles of the fluid are dragged from the hot to the cold surface. Thus, the particles of the fluid moved back from the surface, which is heated, and consequently, $\phi(Y)$ increases.

The correlation governing kinetic energy of the flow and enthalpy difference is called the Eckert number. Eckert number is used in extraordinary speed compressible flow. The positive Eckert number indicates cooling of the wall, and consequently, the heat transmission convection to the fluid is intensified.

The higher Brownian motion causes arbitrary motion of the particles. Due to this arbitrary motion, extra heat is created. Thus, escalation in temperature filed is depicted.

In thermophoresis phenomena, the small particles of the fluid are dragged from the hot to the cold surface. Thus, the particles of the fluid moved back from the surface, which is heated, and consequently, $\theta(Y)$ increases.

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Table 1: Numerical values of the skin friction for various parameters

н	Es	М	$C_{f2} = \frac{1}{Re} V'(-1)$
0.5	0.6	0.6	-0.407027
0.6	0.6	0.6	-0.400427
0.7	0.6	0.6	-0.392627
0.5	0.6	0.6	-0.407027
0.5	0.7	0.6	-0.382364
0.5	0.8	0.6	-0.357702
0.5	0.6	0.6	-0.407027
0.5	0.6	0.7	-0.400893
0.5	0.6	0.8	-0.403960

 Table 2: Numerical values of Nusselt number for different parameters

Rd	Nb	Nt	Pr	−θ ′(−1)
0.5	0.6	0.6	0.7	-1.31073
0.6	0.6	0.6	0.7	-1.27073
0.7	0.6	0.6	0.7	-1.23073
0.5	0.6	0.6	0.7	-1.31073
0.5	0.7	0.6	0.7	-1.52740
0.5	0.8	0.6	0.7	-1.41907
0.5	0.6	0.6	0.7	-1.31073
0.5	0.6	0.7	0.7	-1.52740
0.5	0.6	0.8	0.7	-1.41907
0.5	0.6	0.6	0.7	-1.31073
0.5	0.6	0.6	0.8	-1.31380
0.5	0.6	0.6	0.9	-1.31227

Table 3: Numerical values of Sherwood number for different parameters

Pe	Nb	Nt	Re	- \$ '(-1)
0.5	0.6	0.6	0.5	0.293560
0.6	0.6	0.6	0.5	0.294480
0.7	0.6	0.6	0.5	0.295400
0.5	0.6	0.6	0.5	0.293560
0.5	0.7	0.6	0.5	0.273971
0.5	0.8	0.6	0.5	0.277900
0.5	0.6	0.6	0.5	0.293560
0.5	0.6	0.7	0.5	0.374567
0.5	0.6	0.8	0.5	0.462067
0.5	0.6	0.6	0.5	0.293560
0.5	0.6	0.6	0.6	0.293560
0.5	0.6	0.6	0.7	0.294480

The Pr has opposite impacts on the temperature of the fluid flow. The higher Pr reduces while the lower Pr increases the fluid temperature. Thus, the fluid temperature reduces with small Prandtl numbers.

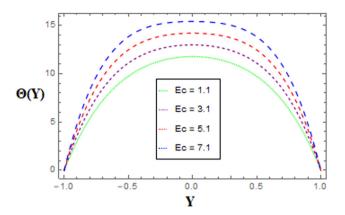


Figure 11: Variations in temperature distribution $\theta(Y)$ for different values of Ec.

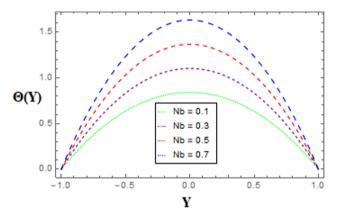


Figure 12: Disparities in temperature distribution $\theta(Y)$ for different values of Nb.

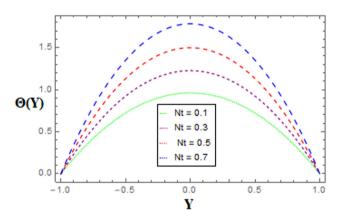


Figure 13: Variations in temperature distribution $\theta(Y)$ for different values of Nt.

The numerical calculations of surface drag force at different values of Es and M are presented in Table 1. We see that the surface drag force is reduced when Es and Mincrease. The numerical calculation of the heat flux at

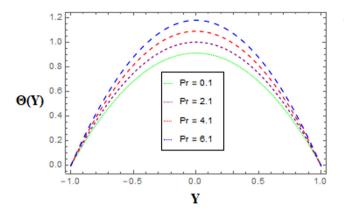


Figure 14: Deviations in temperature profile $\theta(Y)$ for different values of Pr.

different values of Nb, Nt, and Pr is presented in Table 2. With increasing Nb, Nt, and Pr, the heat flux increases. From Table 3, we observe that Sherwood number increases with increasing Nb, Nt, and Re (Figures 11–14).

2 Conclusions

In this article, the behavior of the microchannel nanofluid flow between the two parallel flat plates in the presence of EDL was examined. The Buongiorno nanofluid with body force was assumed. The model equations were solved analytically through HAM. Important model parameters were discussed graphically and numerically. Conclusions are as follows:

- The larger Hartmann number means more collision among the atoms of the fluid, which produces a more resistive force to fluid flow. The more opposing force reduces the fluid flow, and the velocity field falls down.
- Thermal dispersion reduces the heat transmission rate while the salutal dispersion is responsible for the decrease in the mass transmission rate.
- The higher Pr decreases while the lower Pr increases the fluid temperature.
- Temperature field increases the magnitude of Nt as well as the thermophoresis Nb parameters.
- Sharp drop is seen in the nanoparticle concentration profile with an increase in Nt although a small increase is seen with an increase in the value of Nb.
- The result of the viscid indulgence effect on the fluid temperature distribution and the nanoparticle concentration is important. It is because the strength of the shear and the resistance of the friction are significantly increased in the microchannel. It makes the viscous dissipation function strong.

Acknowledgments: The authors extend their thanks to the Deanship of Scientific Research at Majmaah University for funding this work under Project No. (RGP-2019-3).

Conflict of interest: None.

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